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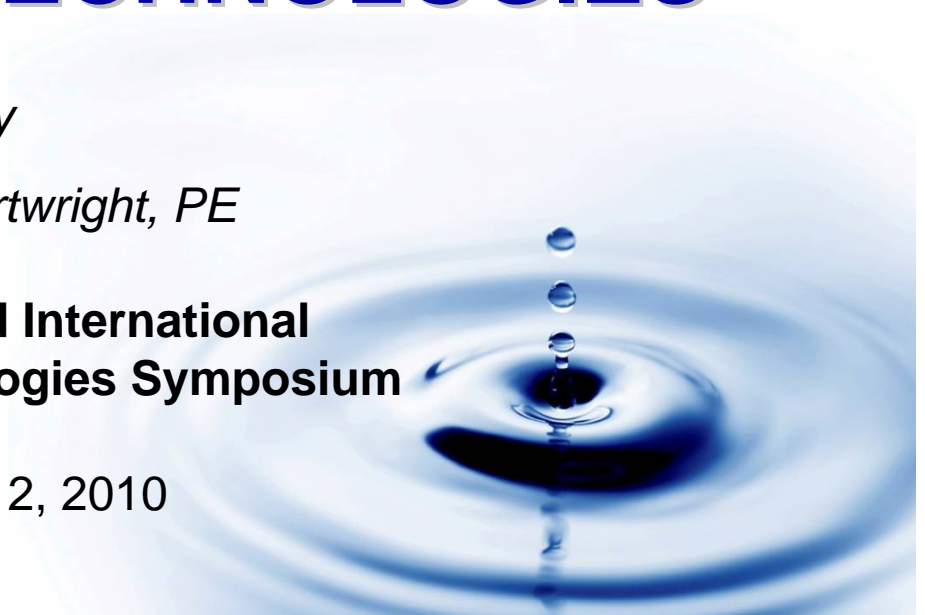
WATER REUSE TECHNOLOGIES

by

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**IAPMO Second International
Emerging Technologies Symposium**

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Introduction

Of All Water on this Planet:

97% Seawater

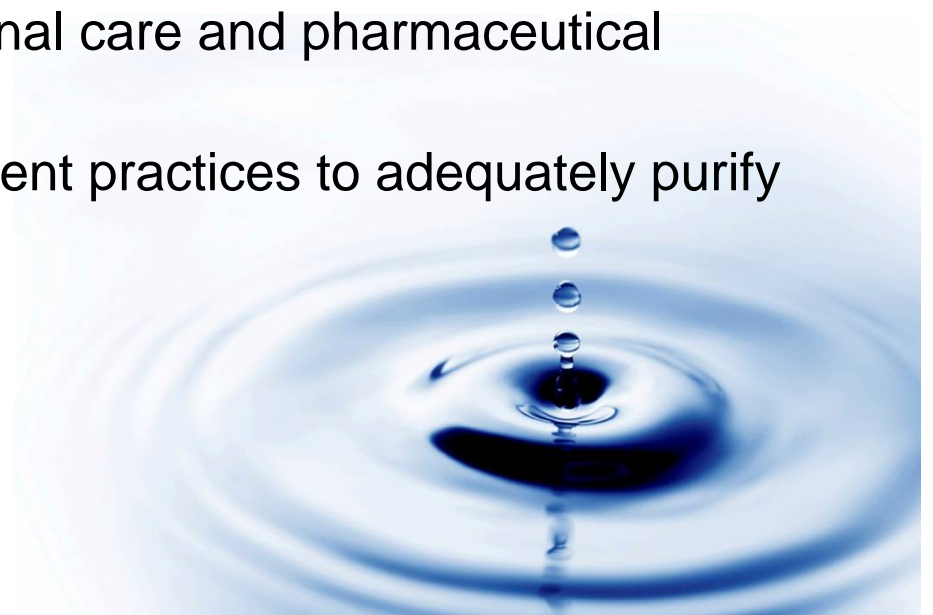
2.4% Glaciers, Ice Caps, Permanent Snow

0.6% Rivers and Lakes



Shortages of Acceptable Quality Due to:

- Steady migration of people into cities (increasing pressure on existing infrastructure).
- Increasing agricultural and industrial activities.
- Economic growth (as standard of living increases, so does per capita water usage).
- Recognition of new, health-related water contaminants, particularly microorganisms and PCPPs (personal care and pharmaceutical products).
- The inability of current water treatment practices to adequately purify water on a large scale.



Reluctance to Embrace Reuse Due to:

- ◆ The “yuck” factor, particularly in reusing biological wastewater.
- ◆ Insufficient knowledge of practical reuse technologies.
- ◆ Economic factors.
- ◆ Lack of commitment.



Water Reuse Mindset:

- ◆ Determine exactly what contaminants are present, along with their concentrations.
- ◆ Determine the quality of water required for reuse.
- ◆ Test and implement the optimum technologies to treat the wastewater for reuse.



Waterborne Contaminants

Class	Examples
Suspended solids	Dirt, clay, colloidal materials, silt, dust, insoluble metal oxides and hydroxides
Dissolved organics	Trihalomethanes, synthetic organic chemicals, humic acids, fulvic acids
Dissolved ionics (salts)	Heavy metals, silica, arsenic, nitrate, chlorides, carbonates
Microorganisms	Bacteria, viruses, protozoan cysts, fungi, algae, molds, yeast cells
Gases	Hydrogen sulfide, methane, radon, carbon dioxide



Water and Wastewater Treatment Technologies

Treatment Technologies	Suspended Solids Removal	Dissolved Organic Removal	Dissolved Salts Removal	Micro-organism Removal
BIOLOGICAL PROCESSES				
MBR (Membrane Bioreactor)	X	—	—	X
Activated sludge	X	X	—	X
Anaerobic digestion	X	X	—	—
Bio-filters	—	X	—	—
EXTENDED AERATION				
Bio-denitrification	—	L	—	—
Bio-nitrification	X	X	—	—
Pasveer oxidation ditch	X	X	—	X
CHEMICAL PROCESSES				
CHEMICAL OXIDATION				
Catalytic oxidation	X	X	—	X
Chlorination	X	X	—	X
Ozonation	—	L	—	X
Wet air oxidation	X	X	—	X
CHEMICAL PRECIPITATION				
CHEMICAL REDUCTION				
Ion exchange	—	—	X	—
Liquid-liquid (solvent)	—	—	X	—
COAGULATION				
Inorganic chemicals	X	X	—	X
Polyelectrolytes	X	X	—	X
ELECTROLYTIC PROCESSES				
Electrodialysis	—	—	X	L
Electrodeionization	—	—	X	—
Electrolysis	—	—	X	—
Ultraviolet irradiation	—	—	—	X
EXTRACTIONS				
INCINERATION				
Fluidized-bed	X	X	—	X
PHYSICAL PROCESSES				
CARBON ADSORPTION				
Granular activated	X	X	—	—
Powdered	X	X	—	X
SPECIALTY RESINS				
FILTRATION				
Diatomaceous-earth filtration	X	—	—	X
Multi-media filtration	X	—	—	X
Micro-screening	X	—	—	X
Sand filtration	X	—	—	X
Flocculation-sedimentation	X	—	—	X
DAF (Dissolved air flotation)	X	X	—	—
Foam separation	X	—	X	—
MEMBRANE PROCESSES				
Microfiltration	X	—	—	X
Ultrafiltration	X	X	—	X
Nanofiltration	X	X	L	X
Reverse osmosis	X	X	X	X
Stripping (air or steam)	X	X	—	—
THERMAL PROCESSES				
Distillation	X	X	X	X
Freezing	—	X	X	—

L = under certain conditions there will be limited effectiveness



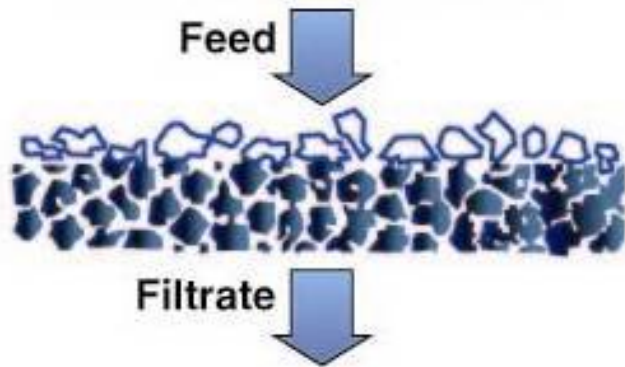
Membrane Technologies

- ▶ Continuous process, resulting in automatic and uninterrupted operation
- ▶ Low energy utilization involving neither phase nor temperature changes
- ▶ Modular design – no significant size limitations
- ▶ Minimal moving parts with low maintenance requirements
- ▶ No effect on form or chemistry of contaminants
- ▶ Discrete membrane barrier to ensure physical separation of contaminants
- ▶ No chemical addition requirements to effect separation

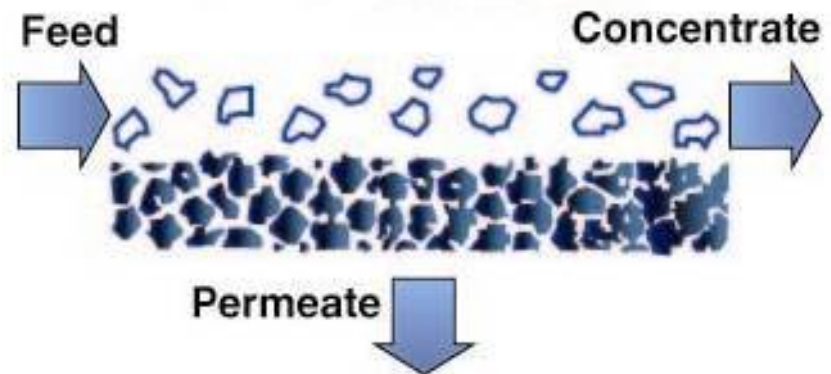


Conventional vs. Crossflow

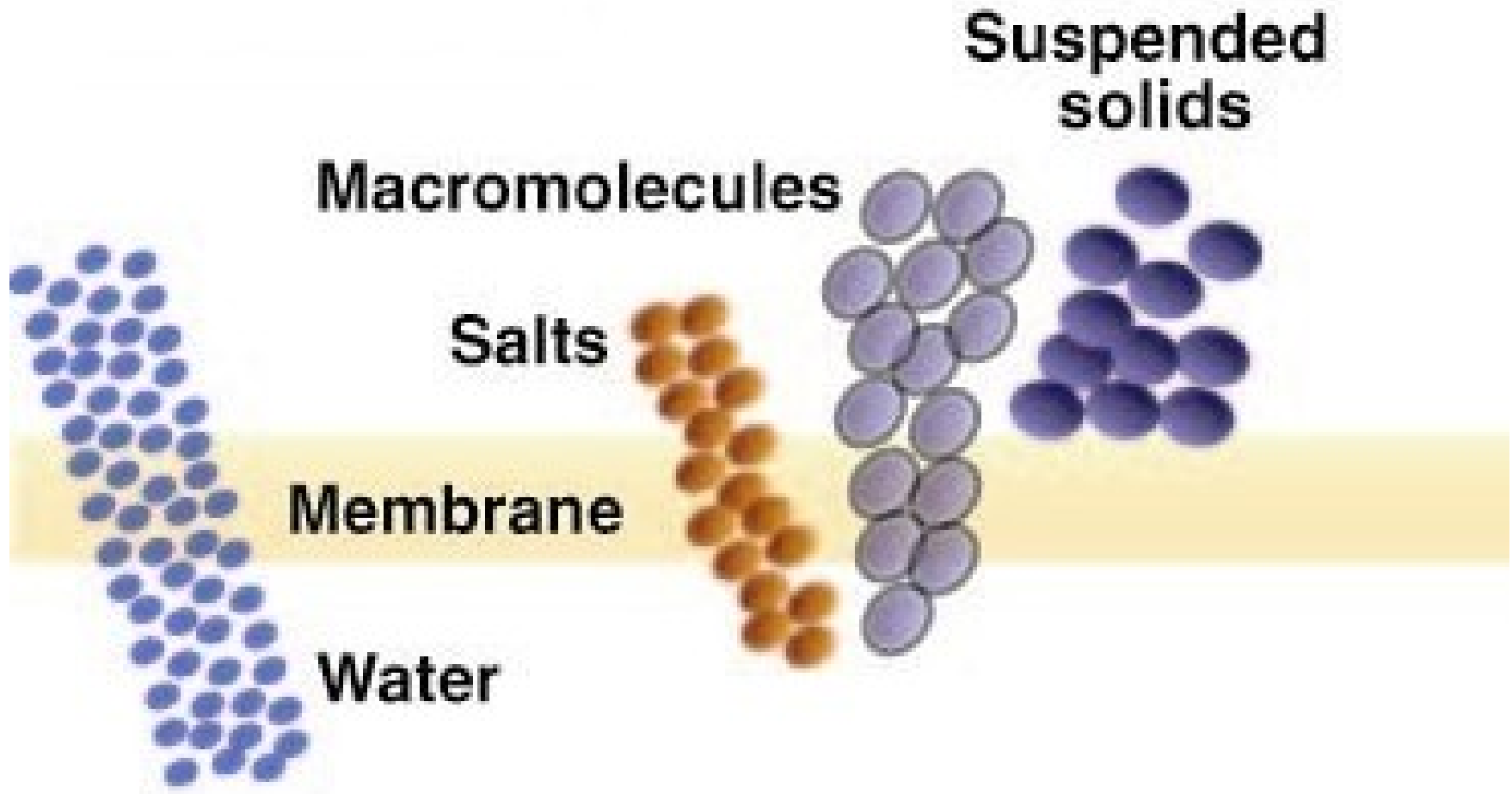
Conventional Filtration



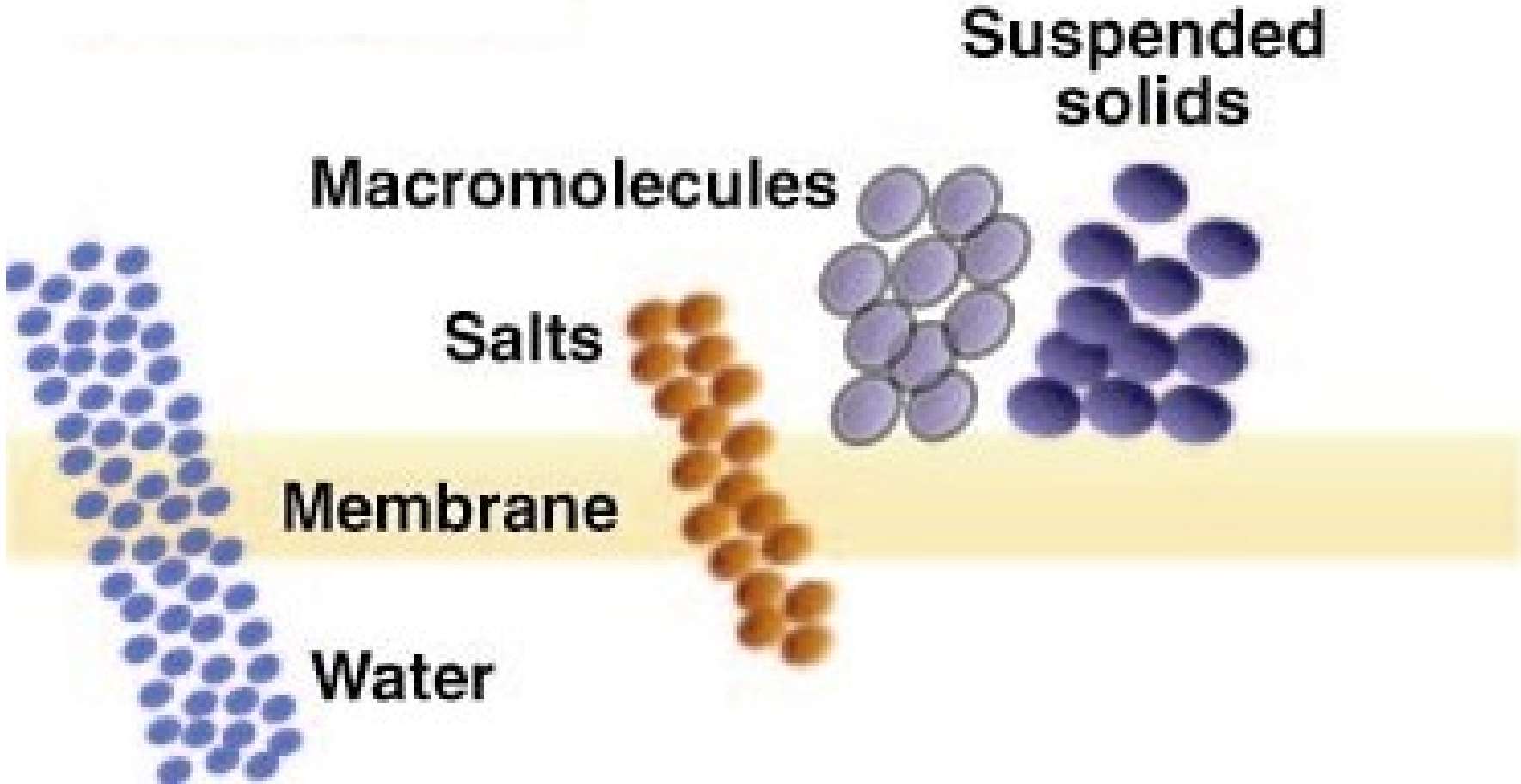
Crossflow Filtration



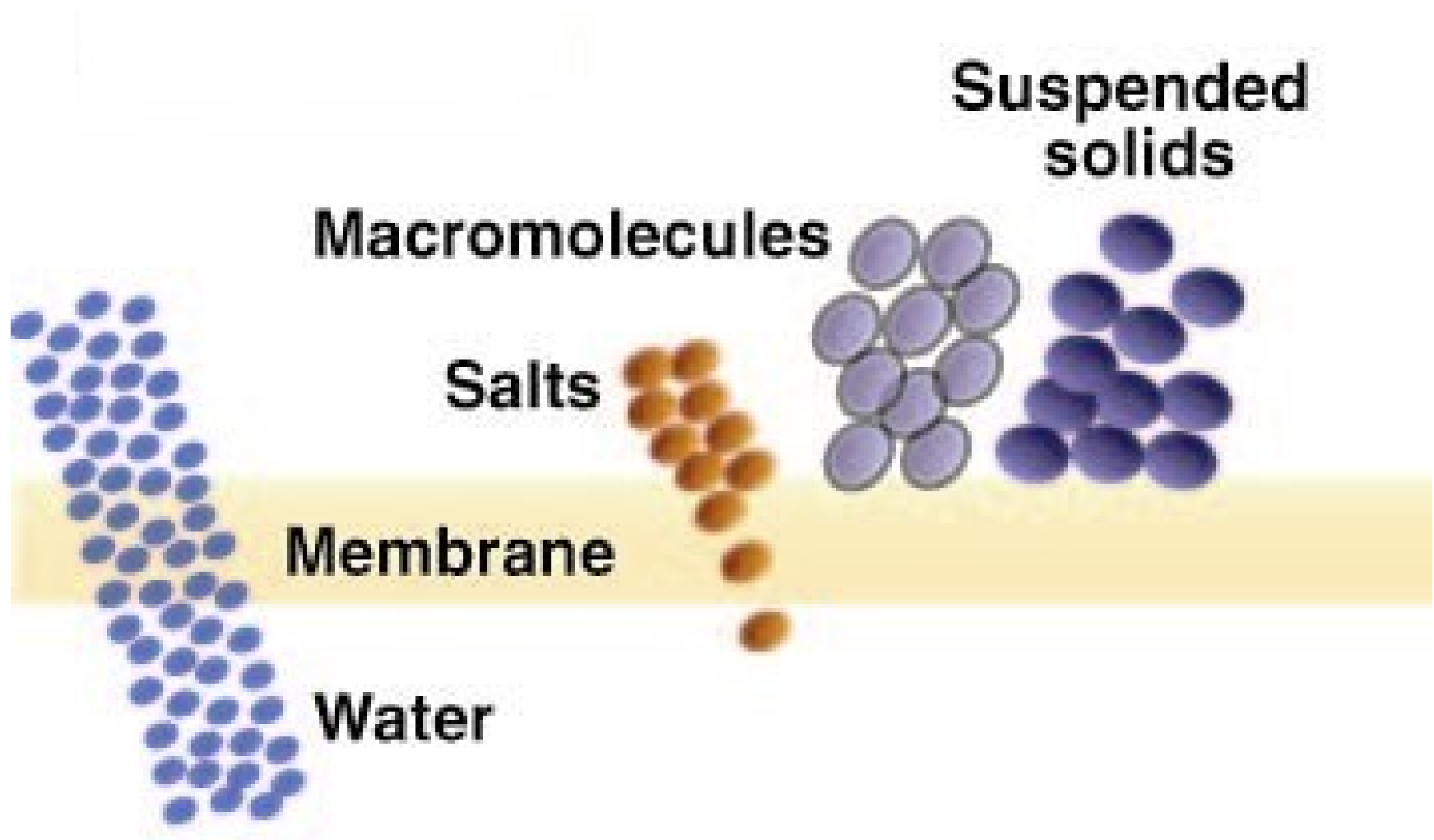
Microfiltration



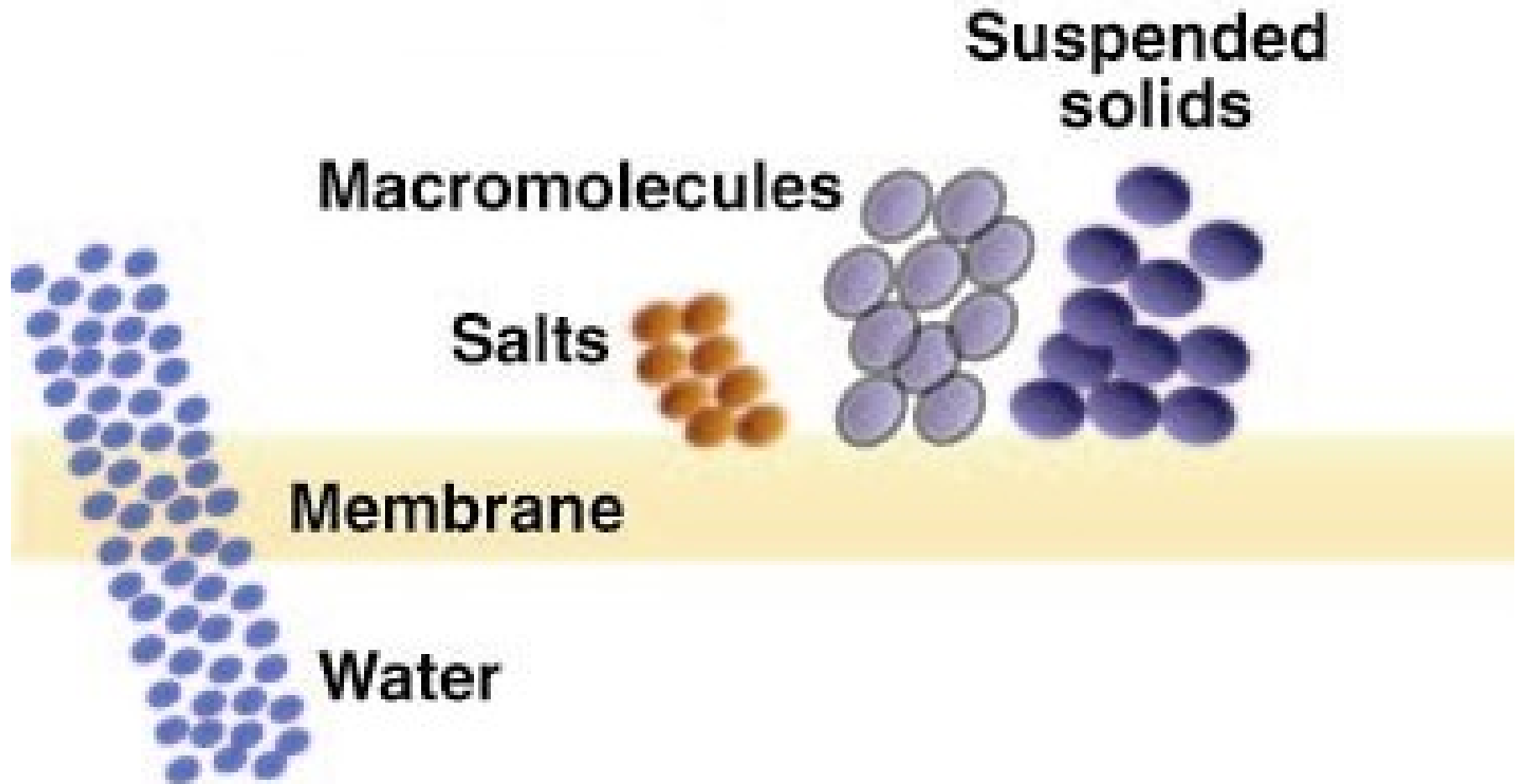
Ultrafiltration



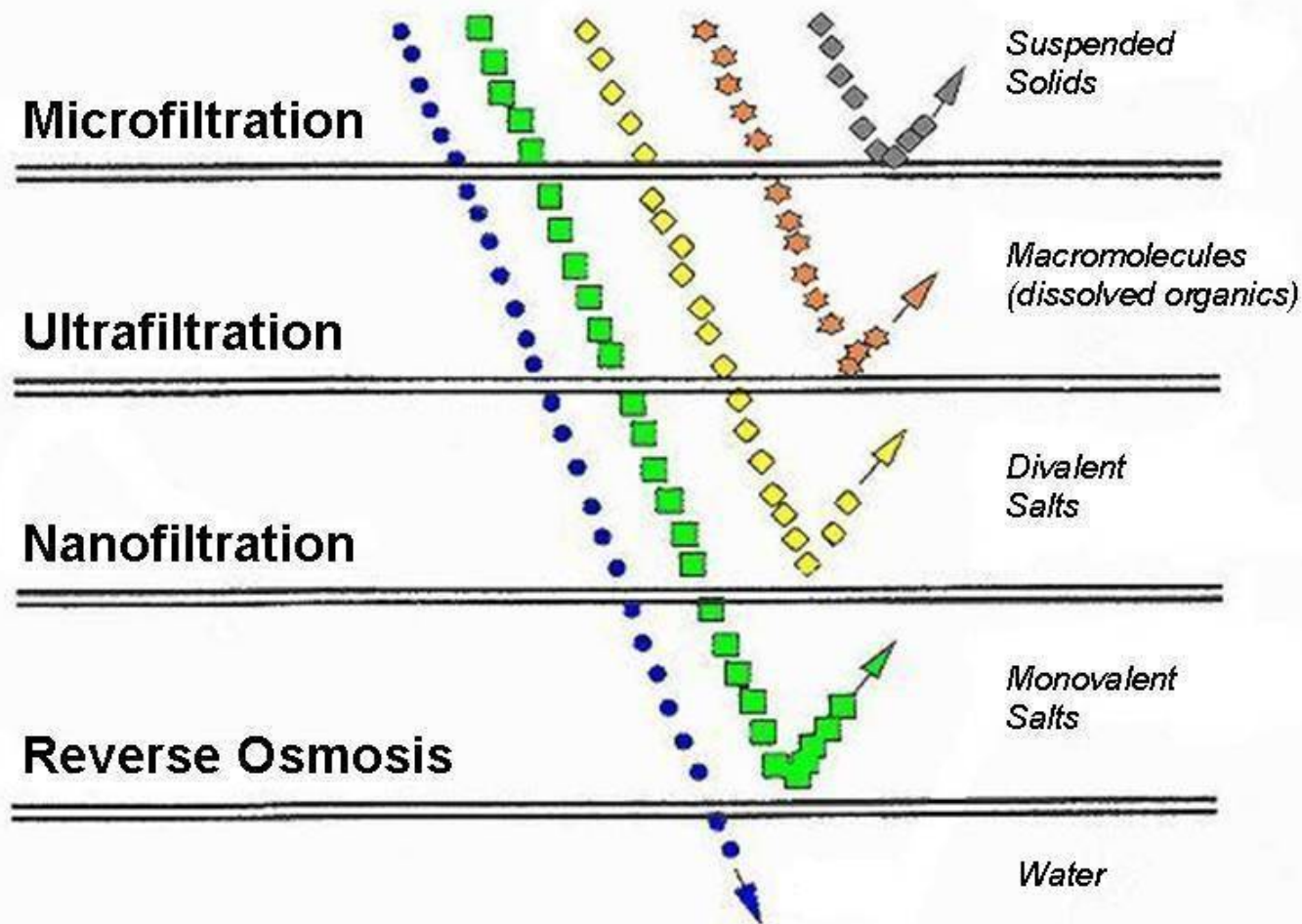
Nanofiltration



Reverse Osmosis



Membrane Separation Technologies

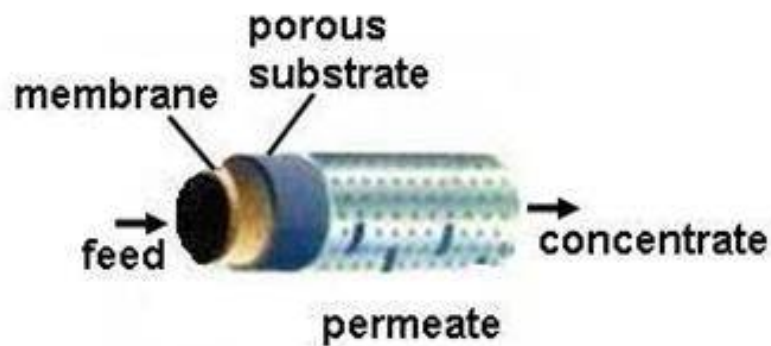


Membrane Technologies Compared

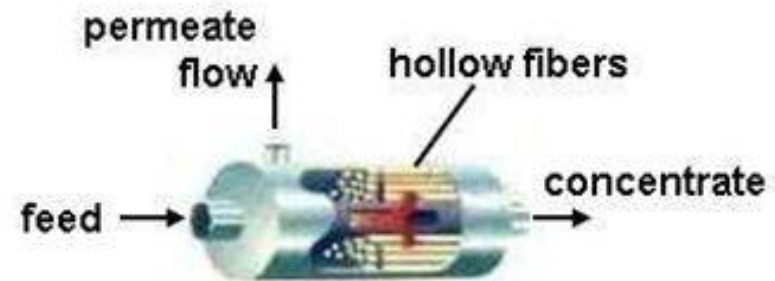
Feature	Microfiltration	Ultrafiltration	Nanofiltration	Reverse Osmosis
Polymers	Ceramics, Sintered metals, Polypropylene, Polysulfone, Polyethersulfone, Polyvinylidene fluoride, Polytetrafluoroethylene	Ceramics, Sintered metals, Polypropylene, Polysulfone, Polyethersulfone, Polyvinylidene fluoride	Thin film composites, Cellulosics	Thin film composites, Cellulosics
Pore Size Range (micrometers)	0.1 - 1.0	0.001 - 0.1	0.0001 - 0.001	<0.0001
Molecular Weight Cutoff Range (Daltons)	>100,000	1,000 - 100,000	300 - 1,000	50 - 300
Operating Pressure Range	<30	20 - 100	50 - 300	225 - 1,000
Suspended Solids Removal	Yes	Yes	Yes	Yes
Dissolved Organics Removal	None	Yes	Yes	Yes
Dissolved Inorganics Removal	None	None	20-95%	95-99+%
Microorganism Removal	Protozoan cysts, algae, bacteria*	Protozoan cysts, algae, bacteria*, viruses	All*	All*
Osmotic Pressure Effects	None	Slight	Moderate	High
Concentration Capabilities	High	High	Moderate	Moderate
Permeate Purity (overall)	Low	Moderate	Moderate-high	High
Energy Usage	Low	Low	Low-moderate	Moderate
Membrane Stability	High	High	Moderate	Moderate

* Under certain conditions, bacteria may grow through the membrane.

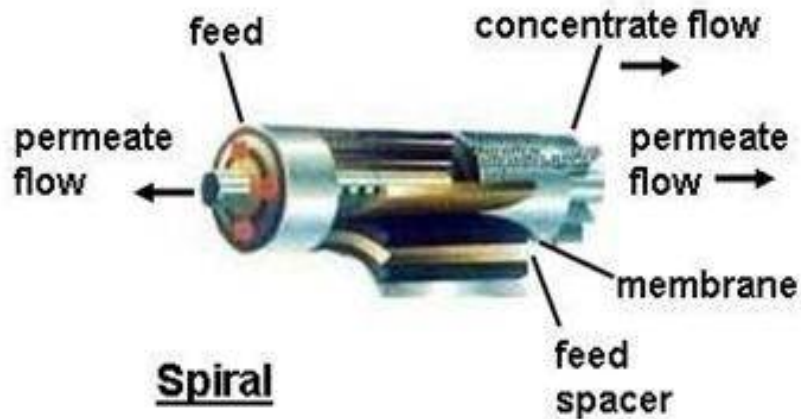
Membrane Element Configurations



Tubular

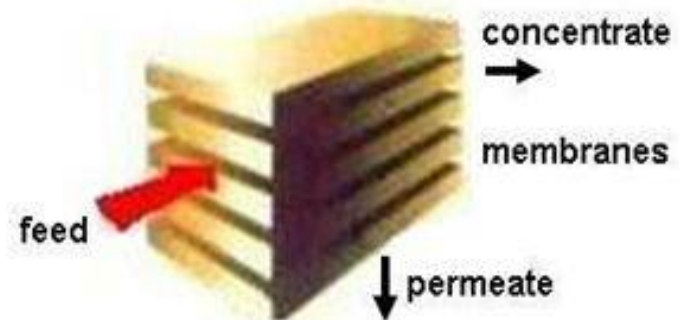


Capillary Fiber

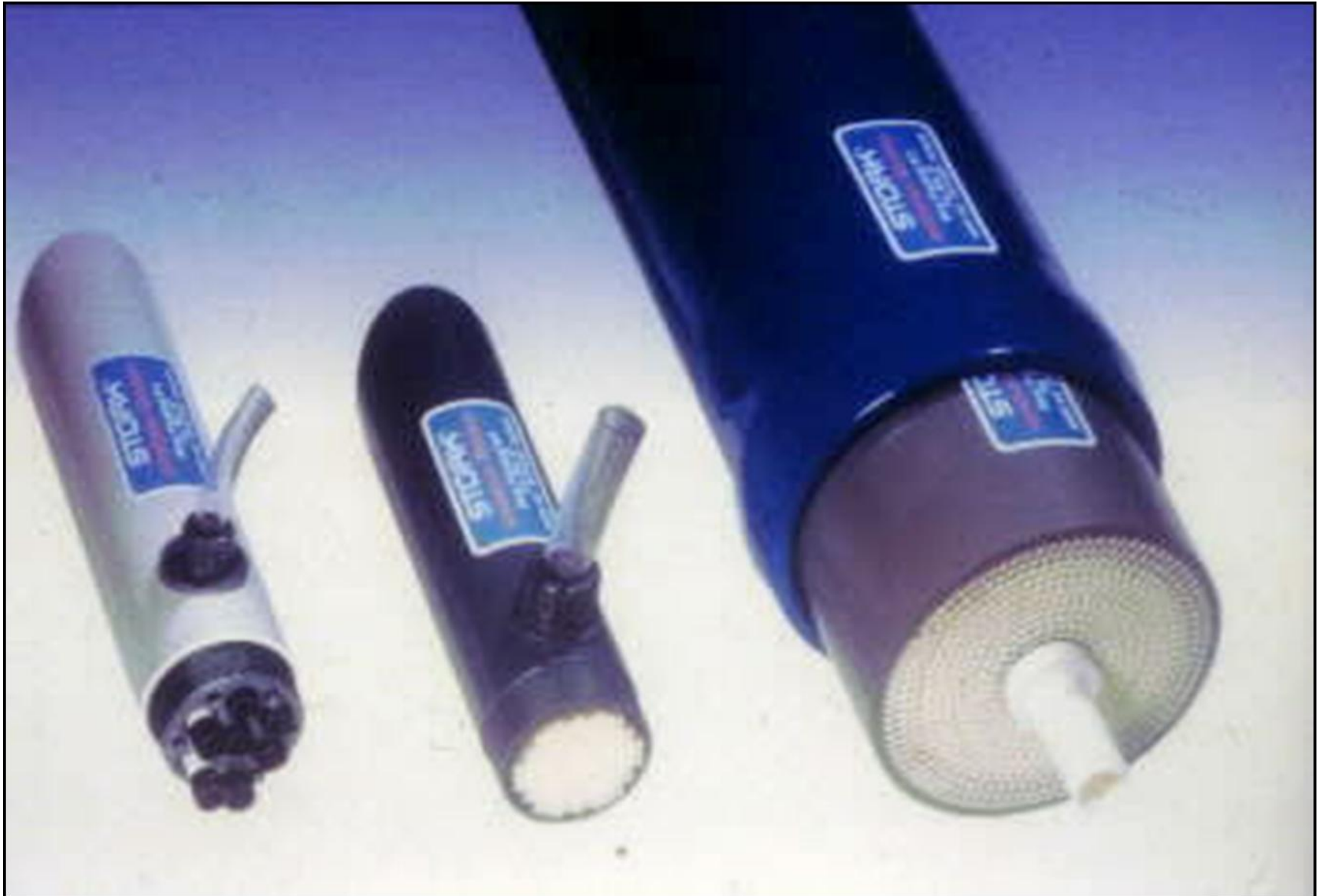


Spiral

Plate and Frame



Tubular



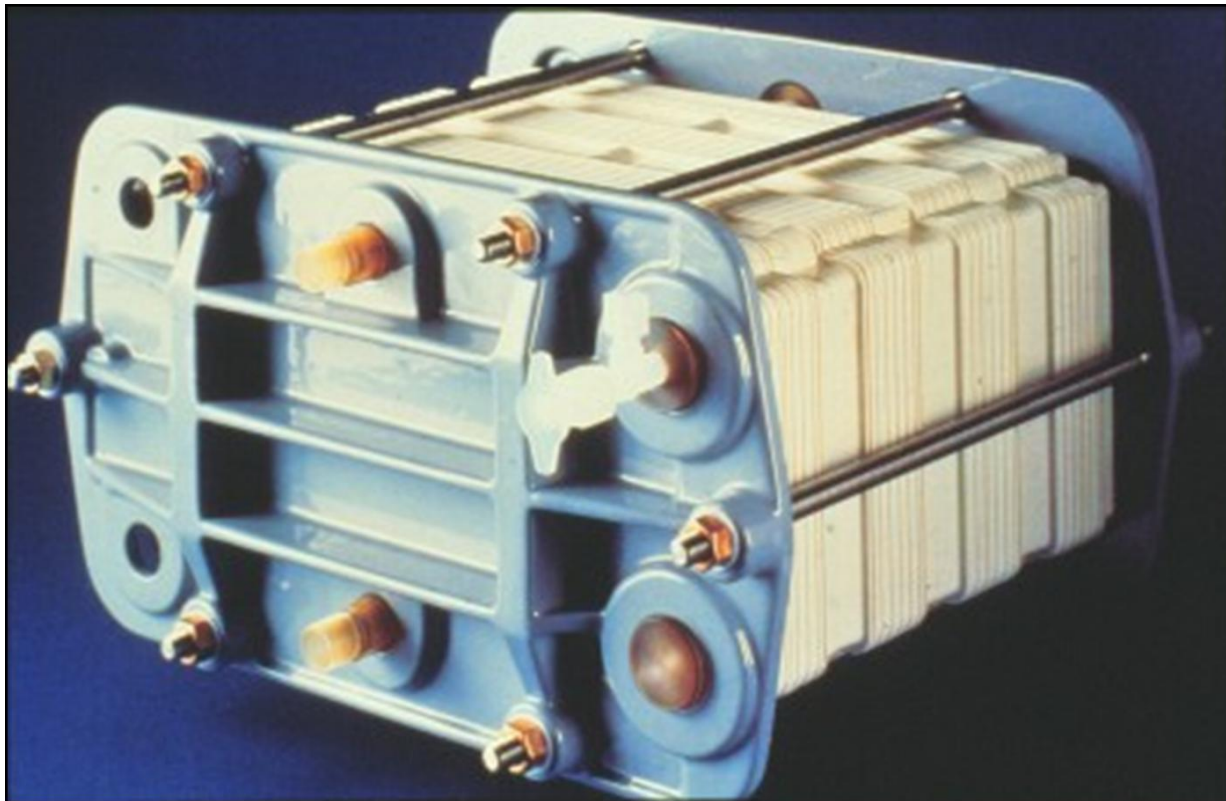
Hollow (Capillary) Fiber



Spiral Wound



Plate and Frame



Membrane Element Configuration Comparison

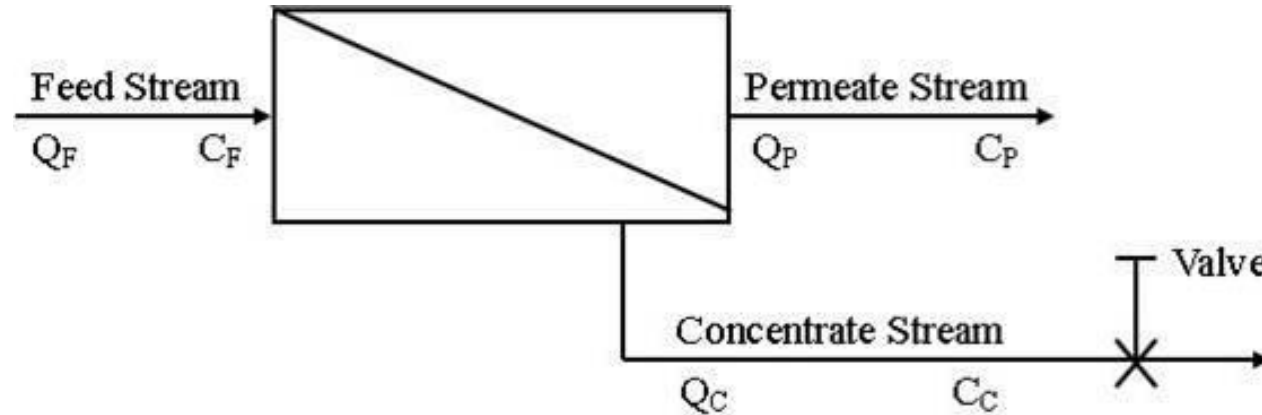
Element Configuration	Packing Density *	Fouling Resistance **
Tubular	Low	High
Hollow (Capillary) Fiber	Medium	Moderate
Spiral Wound	Medium	Low
Plate & Frame	Low	High

* *Membrane area per unit volume of element*

** *Tolerance to suspended solids*



Membrane System Schematic



- Q_F - Feed Flow Rate
- C_F - Solute Concentration in Feed
- Q_P - Permeate Flow Rate
- C_P - Solute Concentration in Permeate
- Q_C - Concentrate Flow Rate
- C_C - Solute Concentration in Concentrate

$$\text{Recovery} = \frac{Q_P}{Q_F}$$

(Expressed as Percent)

TDS = Total Dissolved Solids: Usually considered the total of the ionic contaminants (salts) in solution.

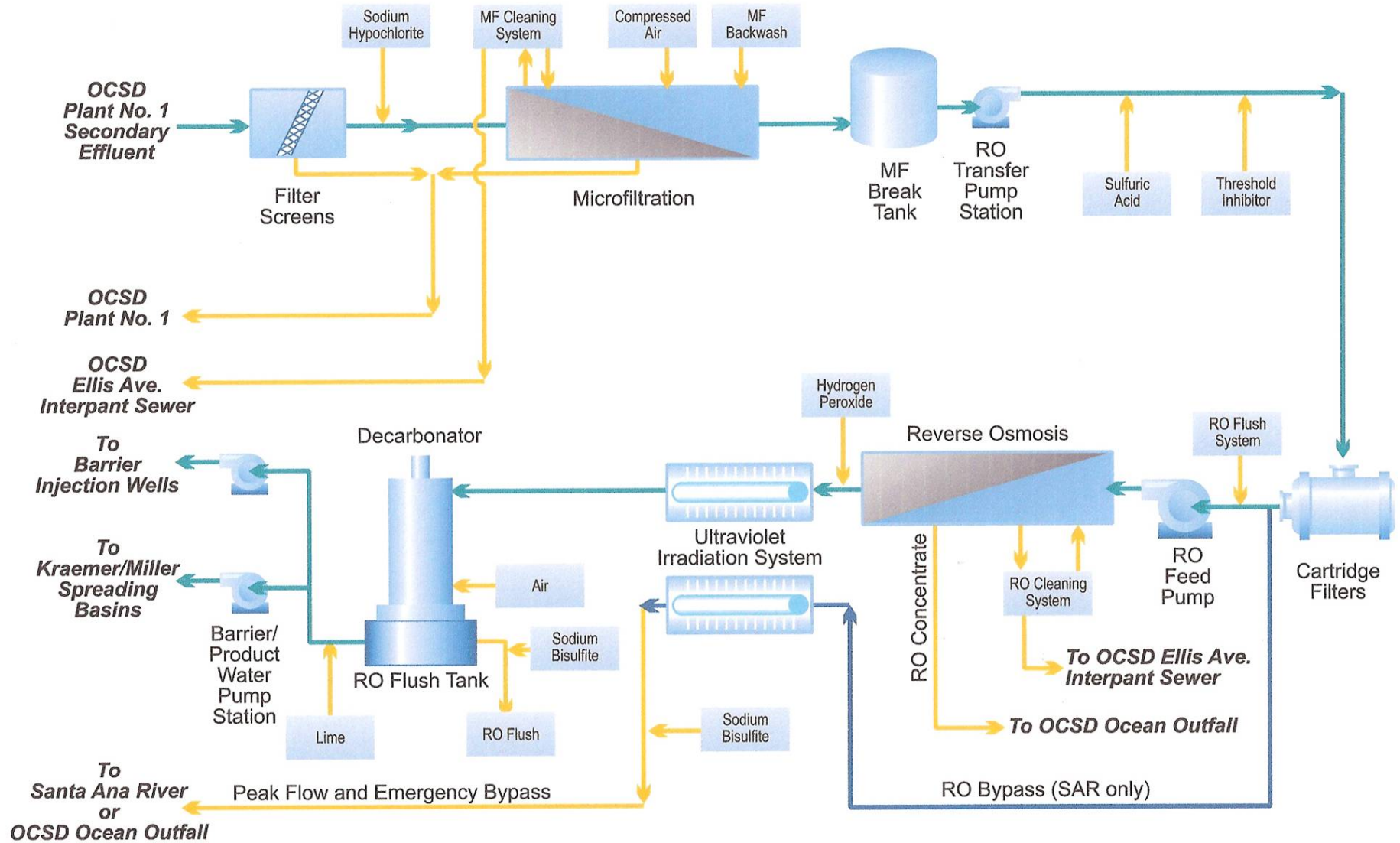
mg/L (milligrams per liter) is the same as ppm (parts per million)

High Recovery Operation

- Higher concentration of contaminants can result in precipitation and greater propensity for fouling.
- In nanofiltration and reverse osmosis applications, the concentrated salts will result in higher osmotic pressure, requiring a higher pressure pump and a more pressure resistant system.
- Also with RO and NF, as recovery is increased, the ionic purity of the permeate decreases.
- As higher recoveries reduce the quantity of concentrate to be discharged, the higher concentration of this concentrate stream can itself present discharge problems.



GWR System



Conclusions

Conservation

Collection

Conversion

Require

COMMITMENT

